

Ondes de Choc dans les Mousses (Blast Waves in Aqueous Foams)

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Introduction

- Blast waves in aqueous foams
 - Strong suppression of blast wave
 - Containment of materials
- Simulation
 - Detonation model
 - Modelling of flow in foam
 - Interface
- 7 equation multi-phase approach
 - Simpler droplet model
- EOS : Quicksteam
 - Also, Quickmethane
- Currently writing 2 journal articles (Quicksteam & VF III)



Motivation : Quicksteam

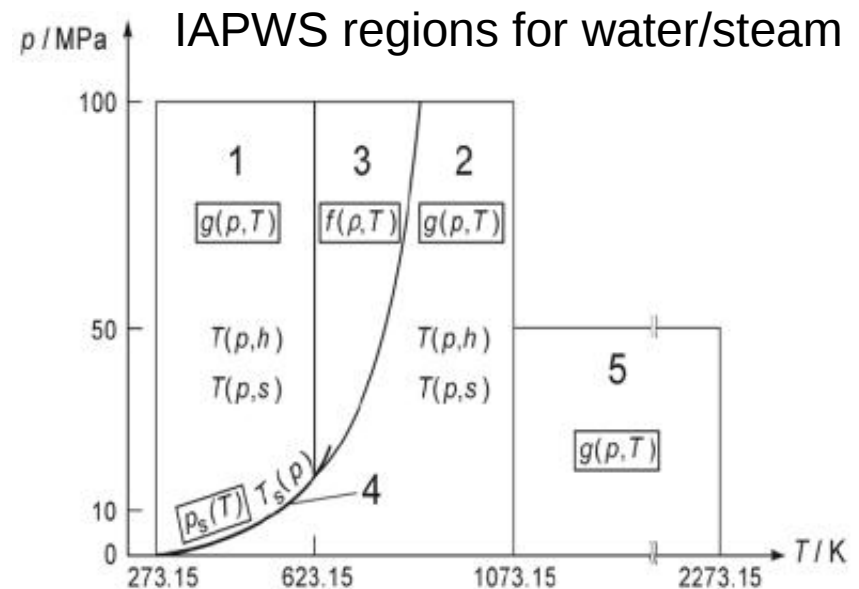
- Ideal gas and stiffened gas laws not good for :
 - Gasses near saturation
 - Liquids
 - Ratio of specific heats $\gamma = C_p / C_v$ not well defined for liquids
- Need more accurate method that better accounts for physics
 - Experimental measurements are well documented and tabulated for water ¹ and methane ²
 - Correlations of the tabulated data allow quick access to properties

1. W. Wagner & H-J Kretzschmar, International Steam Tables, 2nd ed., 1998.

2. U. Setzmann & W. Wagner, J. Phys. Chem. Ref. Data, 20(6), 1991

Quicksteam and Quickmethane

- Quicksteam/methane
 - Correlate equation of state experimental measurements
 - Uses Gibbs or Helmholtz free energy
- Selecting region : Water
 - Region 1, liquid
 - Regions 2 and 5, vapour (steam)
 - Region 3, liquid/vapour
 - Region 4, saturation curve
 - In most cases fixing to region 1 for liquid and 2 for gas will produce the most stable simulation
- Automatic for methane after choice of ρ
- Beyond the region boundaries
 - Necessary in gas/liquid mixtures when temperatures cross saturation curve



The 7 equation Bestion model

- Solve for $v = (\delta, \alpha_g \rho_g, \alpha_l \rho_l, \alpha_g \rho_g U_g, \alpha_l \rho_l U_l, \alpha_g \rho_g E_g, \alpha_l \rho_l E_l)$
- Newton's method to solve equation for T_g, P, T_l

$$R_0 = \frac{(v_0 + v_1)e_a(T_g, P)}{2} + \frac{(v_1 - v_0)e_s(T_g, P)}{2} - v_5 + \frac{v_3^2}{2v_1}$$

$$R_1 = \alpha_l(T_g, P)\rho_l(T_l, P) - v_2$$

$$R_2 = e_l(T_l, P) - \frac{1}{v_2} \left(v_6 - \frac{v_4^2}{2v_2} \right)$$

- Similar equation with R_1 and R_2 for Euler
- Added switch to control phase change

$$Q_{il} = 0 \text{ if } (T_l < T_{\text{sat}} \text{ and } \alpha_v < \alpha_{\text{min}})$$

$$Q_{iv} = 0 \text{ if } (T_g > T_{\text{sat}} \text{ and } \alpha_v > \alpha_{\text{min}})$$

choose $\alpha_{\text{min}} = 10^{-3}$

The 7 equation Bestion model

- Drag force for dispersed phase

$$C_{\text{drag}} = \theta_{\rho} \frac{C^*}{r^*} \frac{\alpha_w \alpha_g \rho_w \rho_g}{\rho} |u_g - u_w|$$

where $\rho \equiv \alpha_g \rho_g + \alpha_w \rho_w$ and $\theta_{\rho} = \rho / (\alpha_g \rho_w)$.

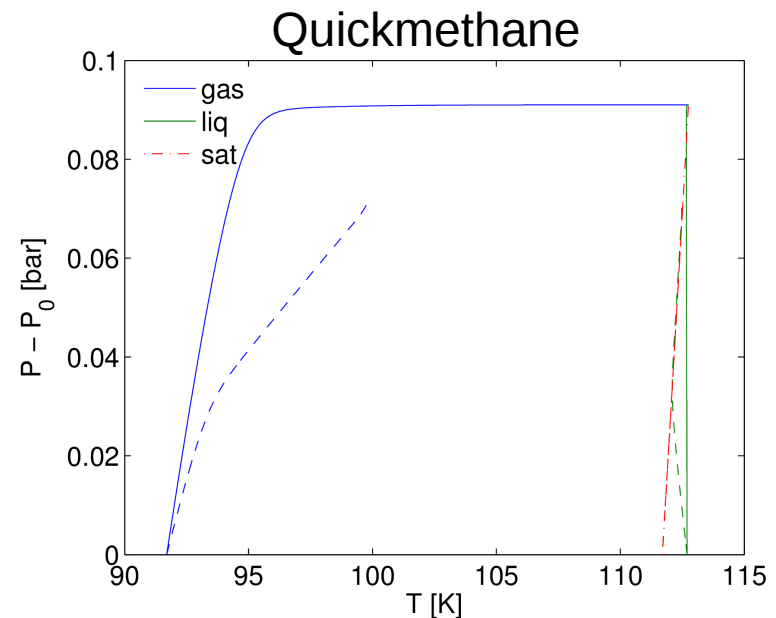
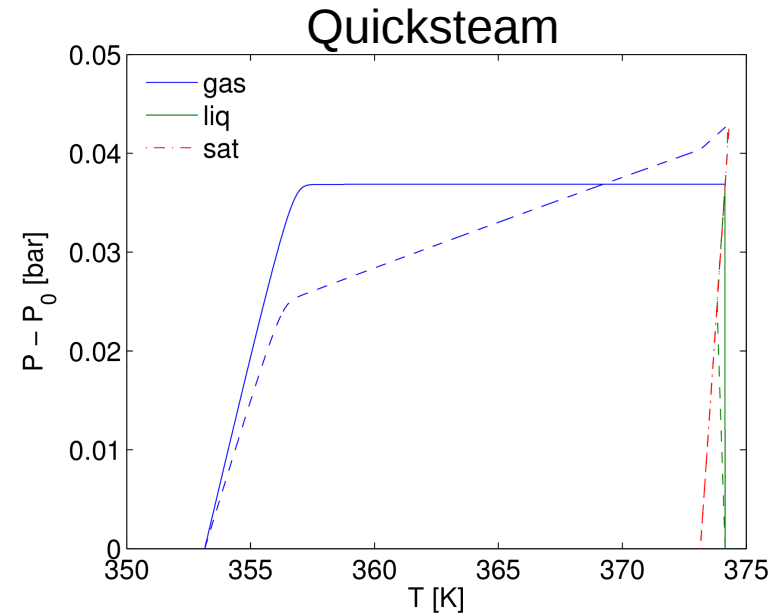
- Dispersed liquid : droplets
- Dispersed gas : bubbles
- When blast wave passes, foam structure destroyed leaving droplets

Test cases

- Return to equilibrium
 - 7 equation Bestion model
- Block of liquid
 - Euler model with interface reconstruction
- Water hammer
 - 7 equation Bestion model

Return to equilibrium

- Intuitive test, looking for correct behaviour
 - i.e. return to saturation curve
- Initially
 - $P_0 = 1.014$ bar
 - $T_l = T_{sat} + 1$
 - $T_g = T_{sat} - 20$
- Single cell, $U_g = U_l = 0$
- Solid : $\alpha_l = \alpha_v = 0.5$, $\alpha_a = 0$
- Dashed : $\alpha_l = \alpha_v = 1/60$, $\alpha_a = 58/60$
- Temperatures return to saturation curve
- Methane (dashed) does not : $\alpha_v \rightarrow 0$



Block of water

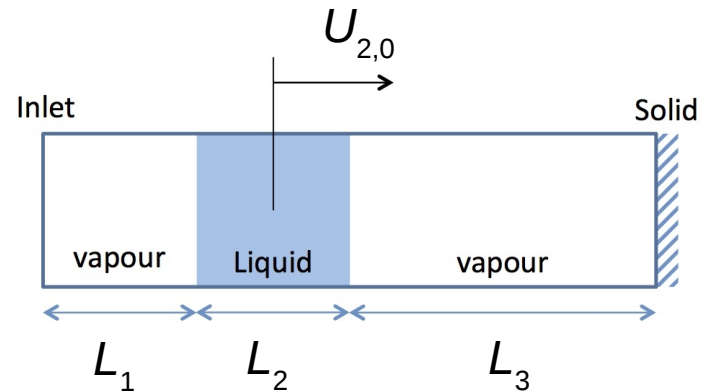
- Tests compressibility effects

- With Interface capturing between liquid and vapour

- Condensate

- Dimensionless groups

- Bagnold number $S = \frac{\rho_L U_{2,0}^2 L_2}{2 P_0 L_3}$

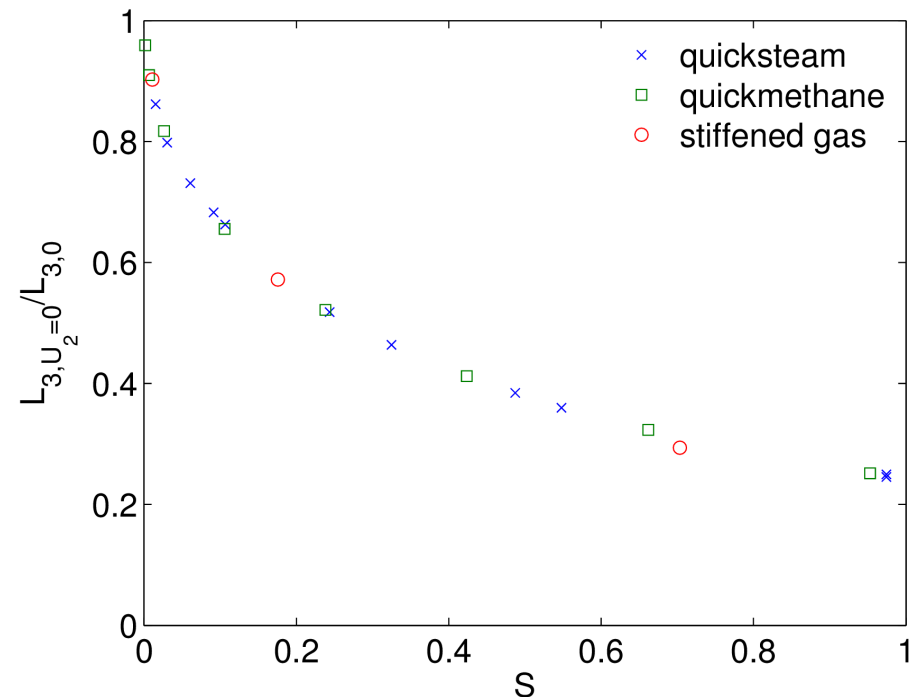


Collapse using Bagnold number

- Range of $U_{2,0}$, L_2 , L_3
 - Quicksteam
 - Quickmethane
 - Stiffened gas

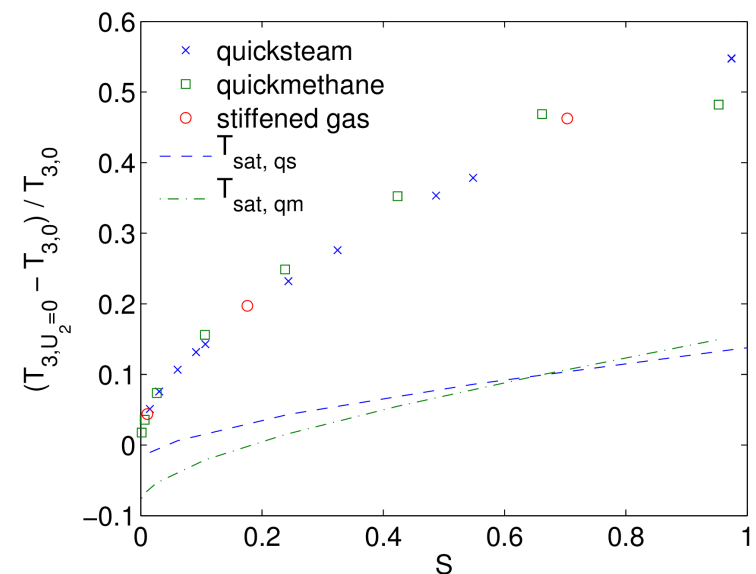
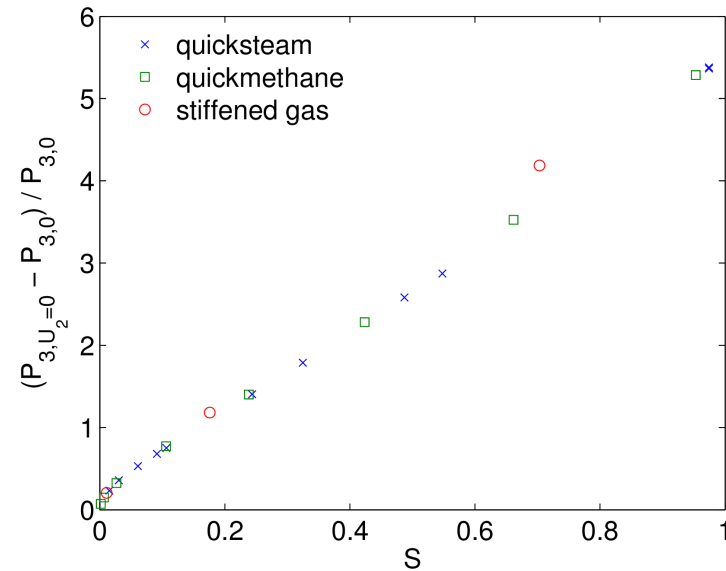
- Bagnold number defined as :

$$S = \frac{\rho_L U_{2,0}^2 L_2}{2 P_0 L_3}$$



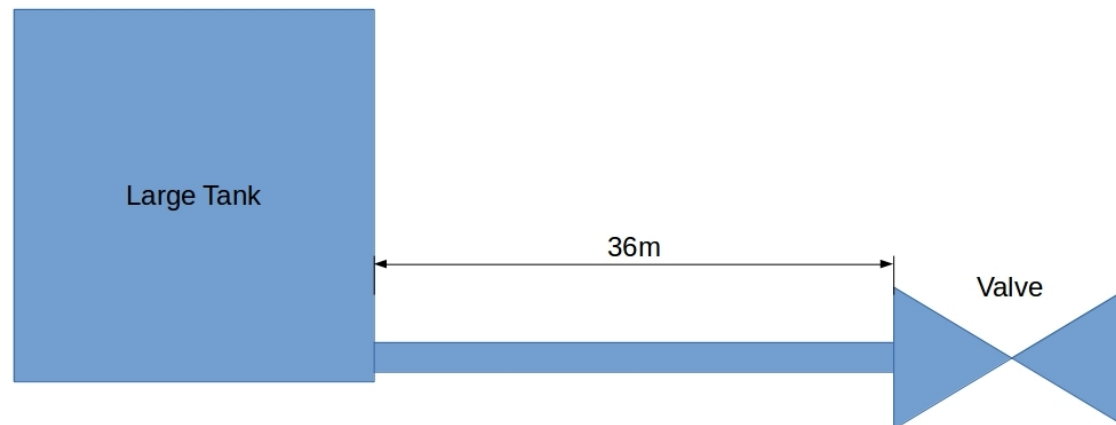
Pressure and temperature

- Properties approx constant inside each separate fluid
- Collapse with Bagnold
- $T_3 > T_{\text{sat}}$
 - No phase change



Water hammer

- Tank connected to a pipe with valve at end
 - Valve is suddenly closed
 - Pressure wave propagates back towards the tank and is reflected
 - Phase change possible depending on initial parameters

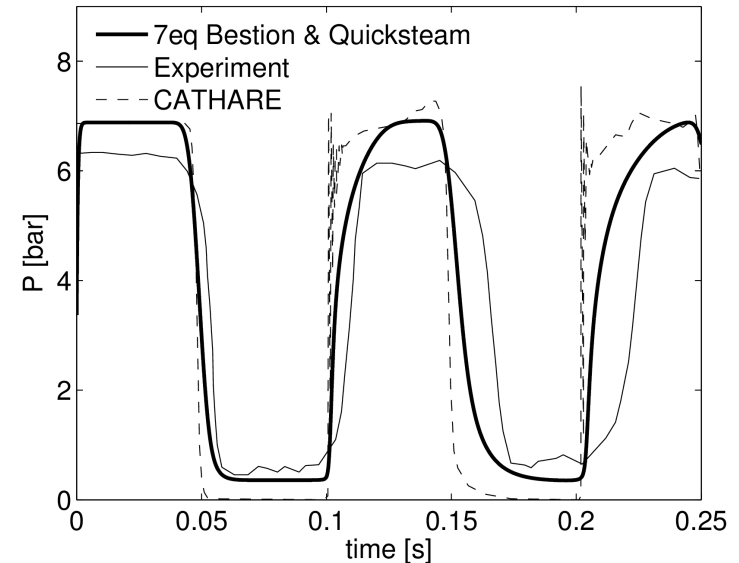


Water hammer

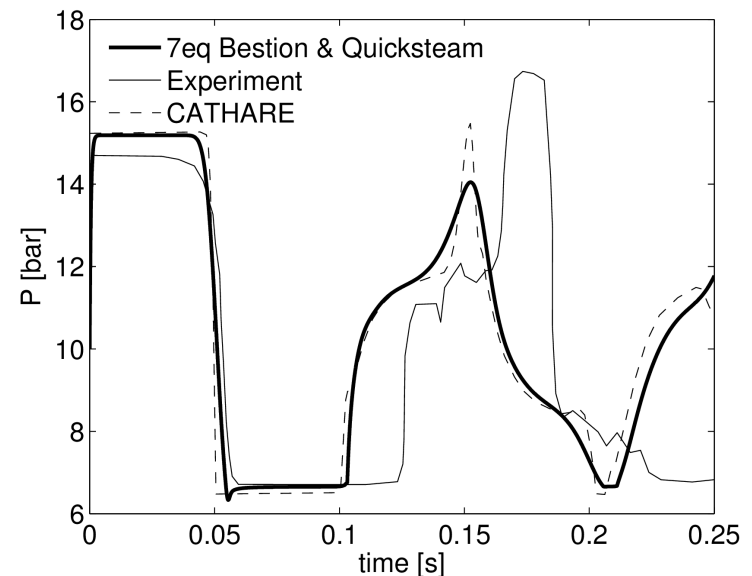
- Experimental and simulation results available ²
- Good match with CATHARE code
 - CATHARE also uses steam tables
 - No phase change $P_{\min}$ higher than CATHARE code
- Match to experimental data can be improved by altering initial condition to account for physical effects ²

2. G. Serre & D. Bestion, Two-Phase Water-Hammer Simulation with the CATHARE Code, 9th International Conference on Nuclear Engineering ; Nice, Acropolis (France) ; 8–12th April 2001.

Without phase change



With phase change



Applications

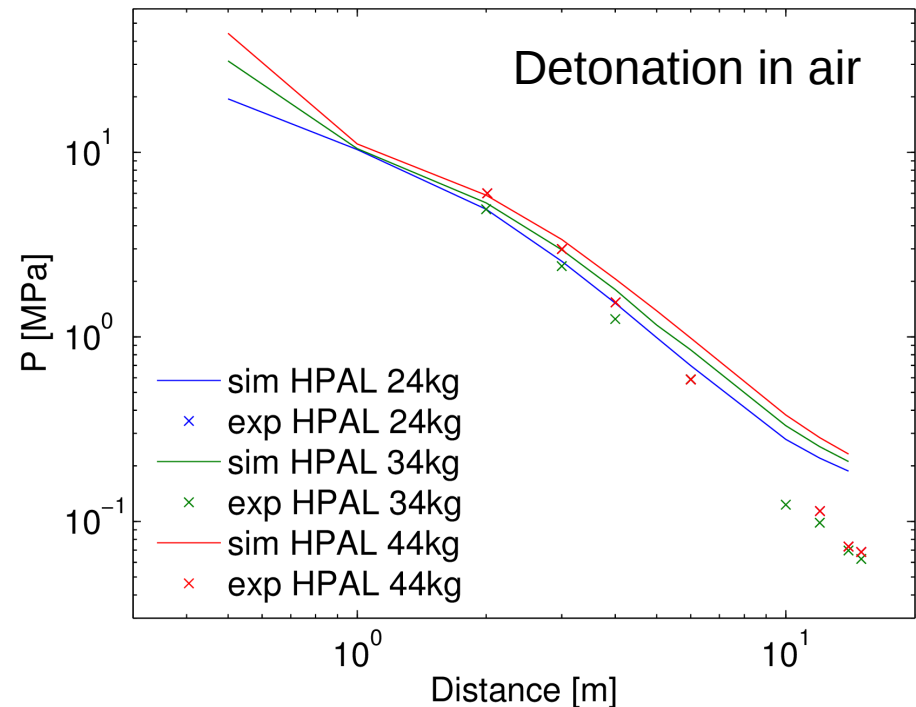
- Article title : Quick recovery of equation of state values for fluid flow simulation using Quicksteam and Quickmethane
- Attenuation of shock waves in aqueous foams
 - Pressures beyond Quicksteam's limits
 - Code not yet capable of these pressures...
 - Could apply stiffened gas or stretch
- Also used to study sloshing methane tanks
 - Liquid compressibility plays important role
 - Work of Matthieu Ancellin

Violent flows III

- Full title 'Violent flow in aqueous foams III: Comparison with experimental measurements and test cases'
- Objective : Make predictions of blast wave attenuation for a given amount of explosive
- Problems
 - Multiple phenomena to be modelled
 - Extremely high pressures
- Test cases
 - Detonation code coupled to Euler solver
 - Shock tube with water droplets
 - Droplet equations
 - 7 equation Bestion
 - Comparison with Sandia correlations

Detonation coupled to Euler code

- Use detonation model of Massoni et al. [3]
- Take data from detonation simulation
- Apply as left boundary condition in Euler simulation
 - Air and water



Shock tube with water droplets

- Experiments from [4]
- Vertical shock-tube
- Water droplets created by jet
- Shock and jet timed to meet at C6
- Strong attenuation of pressure jump

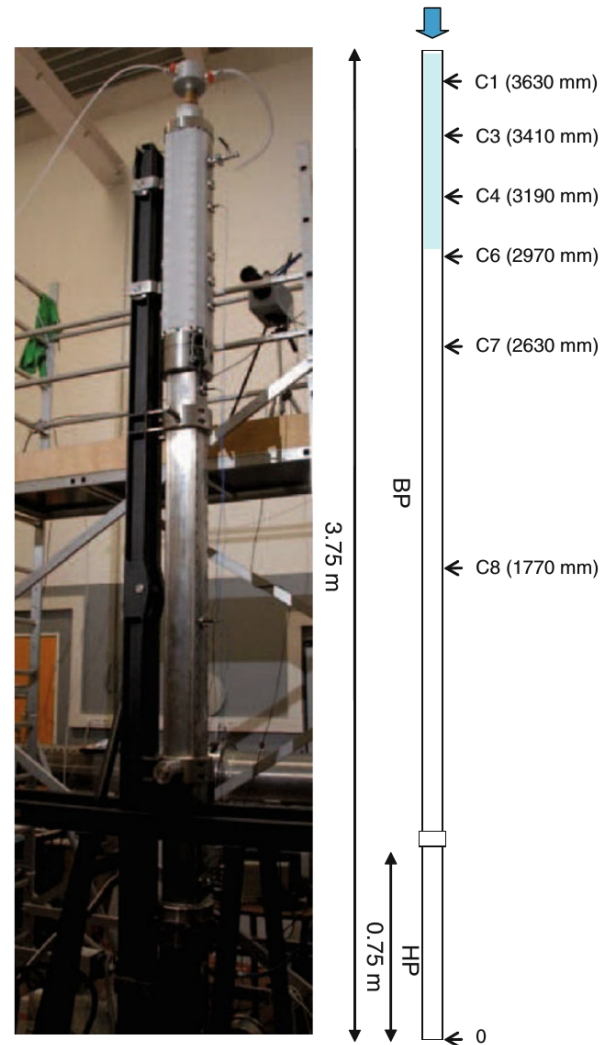
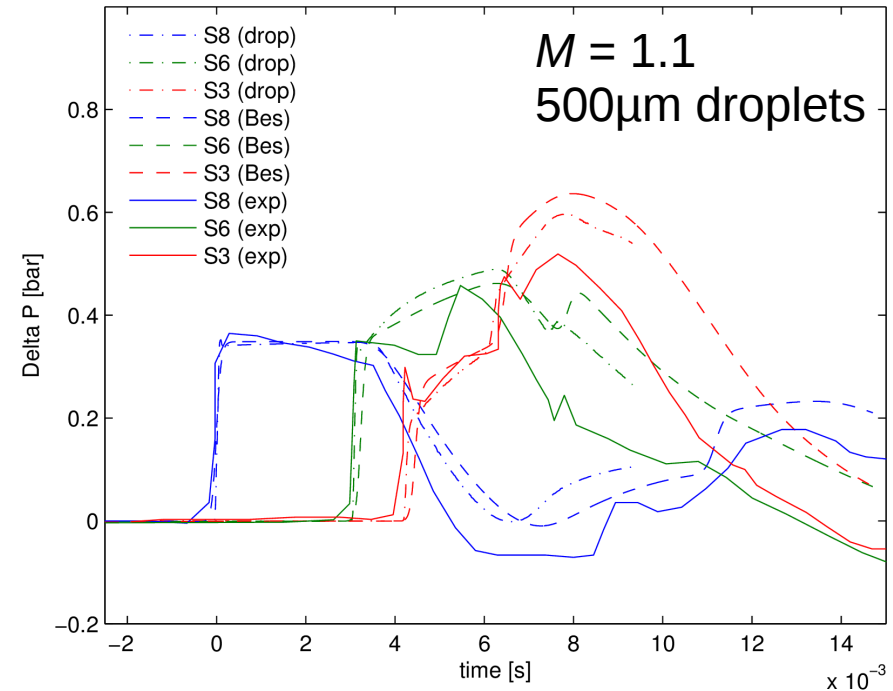


Fig. 6 View of the general experimental set-up and scheme of the shock tube with the locations of the different stations of measurements

Shock tube with water droplets

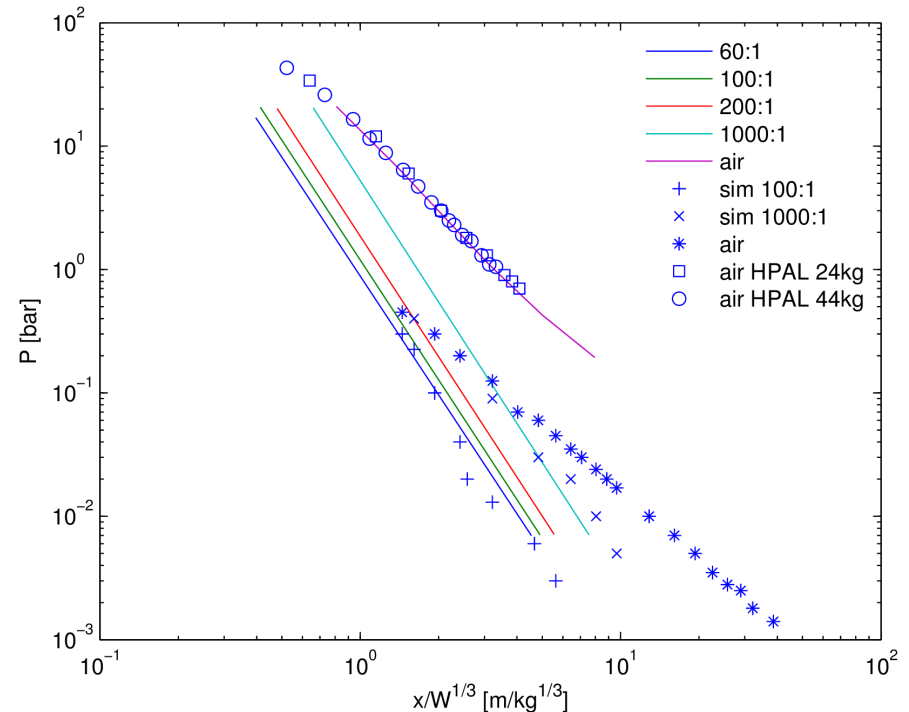
- Varying shock strength, α , and droplet size
- Droplet model used by Jordan et al. [4]
- Results from droplet model and 7 equation Bestion
 - Both models match experiment well at $M = 1.1$



$M = 1.5$ also works, but 1.8 does not. High pressure problem needs to be rectified...

Sandia empirical data fits

- Detonation code at high pressure with Euler
- Low pressure using 7 equation Bestion
- Necessary to control T_g and P behind shock front
 - Negative values
 - using energy and mass sources
 - Would be energy and mass in real explosion



Conclusions

- Quicksteam and Quickmethane improve accuracy and robustness of multiphase simulations
 - 3 test cases
 - Article in preparation
- Good comparison with Sandia correlation for air at high pressure
- Reproduced trend for Sandia foam at low pressure
- Need to increase pressures in 7 equation Bestion model
 - Use numerical solution of Jordan matrix when matrices becomes singular